

- 1.21 The data presented in Example 1.4 in conjunction with the apparatus of Figure 1.11 allowed for finding a convective heat-transfer coefficient. The film coefficient calculated is the one defined in Newton's Law of Cooling. Suppose that we use a different definition for a convective heat-transfer coefficient. Specifically, where T_{wall} is the wall temperature at the inlet, T_{out} is the wall temperature at location 2, T_{in} is the bulk fluid temperature at the inlet, and T_{L} is the bulk fluid temperature at location 2. With the data of Example 1.4, determine the film coefficient \bar{h}_x . Is there any advantage of using this definition over the alternative?

Solution:

$$\dot{m} = 0.5 \text{ kg/s} \quad c_p = 0.2 \times 10^3 \text{ J/(kg}\cdot\text{K)} \quad T_{\text{wall}} = T_{\text{in}} = T_{\text{out}} = 75^\circ\text{C} = \text{constant wall temp.} \\ T_{\text{in}} = 21.4^\circ\text{C} \quad T_{\text{out}} = 20^\circ\text{C} \quad D = 0.025 \text{ m} \quad L = 0.2 \text{ m}$$

$$\dot{q} = \bar{h}_x A [(T_{\text{wall}} - T_{\text{in}}) + (T_{\text{out}} - T_{\text{in}})]$$

$$\dot{m} c_p (T_{\text{out}} - T_{\text{in}}) = \bar{h}_x A [(T_{\text{wall}} - T_{\text{in}}) + (T_{\text{out}} - T_{\text{in}})] \quad \text{Solving,}$$

$$\bar{h}_x = \frac{\dot{m} c_p (T_{\text{out}} - T_{\text{in}})}{A [(T_{\text{wall}} - T_{\text{in}}) + (T_{\text{out}} - T_{\text{in}})]}$$

$$\bar{h}_x = \frac{2(0.5)(0.200)(21.4 - 20)}{\pi(0.025)(0.2)[(75 - 21.4) + (20 - 21.4)]}$$

$$\boxed{\bar{h}_x = 3.546 \text{ W/(m}^2\cdot\text{K)}} \quad \square$$

This coefficient does not require more temperatures to be measured than is more cumbersome to use than the other.

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Table of Contents Janna Heat Transfer Solution Manual

1. Understanding the eBook Janna Heat Transfer Solution Manual
 - The Rise of Digital Reading Janna Heat Transfer Solution Manual
 - Advantages of eBooks Over Traditional Books
2. Identifying Janna Heat Transfer Solution Manual
 - Exploring Different Genres
 - Considering Fiction vs. Non-Fiction
 - Determining Your Reading Goals
3. Choosing the Right eBook Platform
 - Popular eBook Platforms
 - Features to Look for in an Janna Heat Transfer Solution Manual
 - User-Friendly Interface
4. Exploring eBook Recommendations from Janna Heat Transfer Solution Manual
 - Personalized Recommendations
 - Janna Heat Transfer Solution Manual User Reviews and Ratings
 - Janna Heat Transfer Solution Manual and Bestseller Lists
5. Accessing Janna Heat Transfer Solution Manual Free and Paid eBooks
 - Janna Heat Transfer Solution Manual Public Domain eBooks

- Janna Heat Transfer Solution Manual eBook Subscription Services
- Janna Heat Transfer Solution Manual Budget-Friendly Options
- 6. Navigating Janna Heat Transfer Solution Manual eBook Formats
 - ePub, PDF, MOBI, and More
 - Janna Heat Transfer Solution Manual Compatibility with Devices
 - Janna Heat Transfer Solution Manual Enhanced eBook Features
- 7. Enhancing Your Reading Experience
 - Adjustable Fonts and Text Sizes of Janna Heat Transfer Solution Manual
 - Highlighting and Note-Taking Janna Heat Transfer Solution Manual
 - Interactive Elements Janna Heat Transfer Solution Manual
- 8. Staying Engaged with Janna Heat Transfer Solution Manual
 - Joining Online Reading Communities
 - Participating in Virtual Book Clubs
 - Following Authors and Publishers Janna Heat Transfer Solution Manual
- 9. Balancing eBooks and Physical Books Janna Heat Transfer Solution Manual
 - Benefits of a Digital Library
 - Creating a Diverse Reading Collection Janna Heat Transfer Solution Manual
- 10. Overcoming Reading Challenges
 - Dealing with Digital Eye Strain
 - Minimizing Distractions
 - Managing Screen Time
- 11. Cultivating a Reading Routine Janna Heat Transfer Solution Manual
 - Setting Reading Goals Janna Heat Transfer Solution Manual
 - Carving Out Dedicated Reading Time
- 12. Sourcing Reliable Information of Janna Heat Transfer Solution Manual
 - Fact-Checking eBook Content of Janna Heat Transfer Solution Manual
 - Distinguishing Credible Sources
- 13. Promoting Lifelong Learning
 - Utilizing eBooks for Skill Development
 - Exploring Educational eBooks

14. Embracing eBook Trends

- Integration of Multimedia Elements
- Interactive and Gamified eBooks

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