

- 1.21 The data presented in Example 1.4 in conjunction with the apparatus of Figure 1.11 allowed for finding a convective heat-transfer coefficient. The film coefficient calculated is the one defined in Newton's Law of Cooling. Suppose that we use a different definition for a convective heat-transfer coefficient. Specifically, where T_{wall} is the wall temperature at the inlet, T_{out} is the wall temperature at location 2, T_{bulk} is the bulk fluid temperature at the inlet, and T_{bulk} is the bulk fluid temperature at location 2. With the data of Example 1.4, determine the film coefficient \bar{h}_x . Is there any advantage of using this definition over the alternative?

Solution:

$$\dot{m} = 0.3 \text{ kg/s} \quad c_p = 0.2 \times 10^3 \text{ J/(kg}\cdot\text{K)} \quad T_{\text{wall}} = T_{\text{in}} = T_{\text{out}} = 75^\circ\text{C} = \text{constant wall temp.} \\ T_{\text{in}} = 21.4^\circ\text{C} \quad T_{\text{out}} = 20^\circ\text{C} \quad D = 0.025 \text{ m} \quad L = 0.2 \text{ m}$$

$$\dot{q} = \bar{h}_x A [(T_{\text{wall}} - T_{\text{in}}) + (T_{\text{out}} - T_{\text{in}})]$$

$$\dot{m} c_p (T_{\text{in}} - T_{\text{out}}) = \bar{h}_x A [(T_{\text{wall}} - T_{\text{in}}) + (T_{\text{out}} - T_{\text{in}})] \quad \text{Solving,}$$

$$\bar{h}_x = \frac{\dot{m} c_p (T_{\text{in}} - T_{\text{out}})}{A [(T_{\text{wall}} - T_{\text{in}}) + (T_{\text{out}} - T_{\text{in}})]}$$

$$\bar{h}_x = \frac{2(0.3)(0.2)(21.4 - 20)}{0.025(0.3)(75 - 20 + 75 - 21.4)}$$

$$\boxed{\bar{h}_x = 3.546 \text{ W/(m}^2\cdot\text{K)}}$$

This coefficient does not require more temperatures to be measured than is more cumbersome to use than the other.

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